

Original Research Article

<https://doi.org/10.20546/ijcmas.2017.610.135>

Optimization of Saccharification of Biological Pre-Treated Rice Straw by Response Surface Methodology

Pardeep Kaur^{1*}, Gurvinder Singh Kocher¹ and Monica Sachdeva Taggar²

¹Department of Microbiology, Punjab Agricultural University, Ludhiana 141004, Punjab, India

²School of Renewable Energy Engineering, Punjab Agricultural University, Ludhiana 141004, Punjab, India

*Corresponding author

ABSTRACT

Keywords

Rice straw, Fungal consortium, Saccharification, Bioethanol, Response surface methodology.

Article Info

Accepted:
10 September 2017
Available Online:
10 October 2017

Pretreatment of rice straw facilitating the enzymatic saccharification process was performed by a ligninolytic fungal consortium, resulting in rice straw having 56.4 % cellulose, 12.2% hemicelluloses, and 2.2% lignin. Using response surface methodology, the combined effect of substrate concentration, temperature and pH on reducing sugar yield from enzymatic saccharification of rice straw optimized substrate concentration, 5.0% (w/v); temperature, 55°C and pH, 4.8 yielding a maximum sugar content of 492.0 milligram per gram dry substrate (mg/gds) with a saccharification efficiency of 81.1%. The experimental results were in good agreement with predicted values. Therefore, the model could be successfully used to identify the effective combinations of the three factors for predicting reducing sugar yield.

Introduction

Lignocellulosic biomass is an attractive and economical feedstock for bioethanol production because of its abundance and renewable nature (El-Ahmady El-Naggar *et al.*, 2014). Rice straw consisting of cellulose (35-40%, w/w), hemicelluloses (20-30%, w/w) and lignin (10-15%, w/w) is one of the most abundant lignocellulosic wastes in the world (Binod *et al.*, 2010). It has been estimated that in India, paddy is cultivated in about 43 million ha producing about 96 million tons of rice and 250 million tons of straw. The options for the disposition of rice straw are limited by the low bulk density, slow degradation in the soil, harbouring of rice stem disease and high mineral content (Kocher *et al.*, 2016).

Nowadays, field burning, though an offense is the major practice for removing rice straw, but it increases the air pollution and consequently affects the public health (Wi *et al.*, 2013).

Pretreatment is essential for removal of lignin and hemicellulose to reduce cellulose crystallinity and increase the porosity of biomass (Zhu *et al.*, 2015). Post pretreatment, the amorphous cellulose is saccharified by the enzymes, and the resulting glucose is fermented to ethanol. Therefore, optimization of saccharification is an important step in the development of an efficient and cost effective saccharification strategy. Further, the traditional 'one-factor-at-a-time approach' is time consuming and does not reveal the interactive effects between the variables for optimization (Qi

et al., 2009). In this regard, response surface methodology (RSM) is an effective tool wherein many factors and their interactions affecting the response can be identified with fewer experimental trials [Box *et al.*, 1978]. The RSM includes three major steps: (1) implementing a statistically designed experimental plan to the data, (2) developing a regression model to correlate experimental data, and (3) predicting the response of target variables to the process parameters using the regression model (Li *et al.*, 2010; Vanderghem *et al.*, 2010).

In the present study, rice straw pretreated with a ligninolytic fungal consortium was to identify the optimum saccharification conditions by using RSM based on a second order Central composite design (CCD).

Materials and methods

Microorganisms

A fungal consortium was developed using *Pleurotus ostreatus*, procured from Department of Microbiology, PAU Ludhiana and *Phanerochaete chrysosporium* MTCC 787 procured from Microbial Type Culture Collection (MTCC), Institute of Microbial Technology (IMTECH) Chandigarh.

Development of ligninolytic consortia

The mycelia of *P. ostreatus* and *P. chrysosporium* were grown on PDA medium. The spores were obtained from one week old Petri plates by rinsing the plates with sterile distilled water and collecting the spores in sterile vials. The spore count was determined with the help of haemocytometer. The fungal spore suspension of 1×10^8 spores/ml was used for inoculation.

Enzyme production

The ligninolytic enzyme production from fungal consortium was carried out under solid state fermentation conditions using paddy straw (500 μ), moistened with lignin modifying enzyme (LME) basal medium (Pointing, 2010) to 80% moisture content. The experimental flasks were autoclaved at 121°C for 15 min, inoculated with

fungal spore suspension (1×10^8 spores/ml) and incubated at 28°C in a BOD incubator.

Enzyme extraction and concentration

The extraction was performed by mixing the contents of experimental flask with 0.1 M potassium phosphate buffer (pH 6.0), added to achieve a solid/ liquid ratio of 1: 10 (w/v). The suspension was stirred at 120 rpm for 30 min in an orbital shaking incubator. The biomass was filtered using Whatman filter paper (No.1) and the filtrates were centrifuged for 10 min at 6000 rpm. The supernatants (crude enzyme extract) was subjected to ultrafiltration using a Polyethersulphone (PES) membrane of 10 KDa molecular weight cut off (CleaN Sep, Pvt. Ltd., Mumbai).

Enzyme assay

The concentrated enzyme extract was assayed for ligninolytic enzyme activity viz. laccase, lignin peroxidase and manganese peroxidase by the methods of Desai *et al.*, (2011); Tien and Kirk (1988) and Paszczynski *et al.*, (1988) respectively.

Pretreatment and proximate analysis of rice straw

The rice straw used in the present study was collected from Demonstration area, School of Renewable Energy Engineering, Punjab Agricultural University, Ludhiana. The washed and sun dried straw was chopped, ground to 2-10 mm and finally sieved to 30 mesh size. The rice straw was pretreated with concentrated (10 folds) enzyme extract under shake flask conditions using 2.5 g rice straw, 8.0 ml concentrated ligninolytic enzyme extract, supplemented with 10 mM Ca^{2+} ions and incubated at 45°C for an incubation period of 72 h (unpublished data). The pretreated biomass samples were analysed for Neutral detergent fibre (NDF), Acid detergent fibre (ADF) and Acid detergent lignin (ADL) by the method of Goering and Van Soest (1970).

Saccharification of pretreated rice straw

Saccharification experiments were performed using commercial cellulase enzyme from

Arrowzymes (Banglore, India). The cellulase (30 FPU/g-substrate) was added to 0.1 M sodium citrate buffer (pH 4.8- 6.8) supplemented with 0.02% (w/v) sodium azide to inhibit microbial contamination, and then mixed to the substrate at a concentration of 5.0 -12.0% (w/v).

The experiments were carried out in 125 ml Erlenmeyer flasks containing 20 ml total reaction volume (the buffer–enzyme mixture). A surfactant, Tween 20 (0.2%) which can enhance the enzymatic conversion of lignocellulosic biomass and does not inhibit cell growth in the downstream fermentation process was used in these saccharification experiments (Sharma *et al.*, 2014). The flasks were incubated at different temperatures (45-55°C) for 48 h in a rotary shaker at 100 rpm. Each sample taken from the saccharified solution was heated to 100°C immediately for 3 min to denature the enzymes, cooled to room temperature, and then centrifuged for 10 min at 6000 rpm. The supernatant was used for reducing sugar analysis (Miller, 1959). The saccharification (%) was determined using the following formula:

$$\text{Saccharification (\%)} = \frac{\text{Amount of reducing sugars formed (g)}}{\text{Amount of cellulose (g)}} \times 0.9 \times 100$$

Statistical design of experiments

To determine the best combination of parameters for optimizing the enzymatic saccharification of rice straw, a second order Central composite design (CCD) was employed. In CCD, the total number of experimental combination were 2^k+2K+n_0 , where K is the number of independent variables and n_0 is the number of repetitions of the experiment at the central point. The CCD contains a total of 20 experimental runs with five level full factorial design and replications of the central and the axial points. The substrate concentration (% w/v), temperature (°C) and pH were selected as independent variables and dependent variable selected was reducing sugar yield (mg/g dry substrate).

The Design-Expert software, version 9.0.4.1 developed by (Stat- Ease Inc., Minneapolis, MN,

USA) was used to build and analyze the experimental design e.g. analysis of variance (ANOVA), determination of the estimated effects and interaction, regression equation which was fitted to the data. Three dimensional surface plots were drawn to show the effects of independent variables on response and a quadratic polynomial equation was proposed to describe the mathematical relationship between the variables and the response. The significance of the model was evaluated by determination of R^2 and adjusted R^2 coefficient. An experiment was also conducted to confirm the predicted optimum response using the selected optimum values of three variables. A second order polynomial equation was used to describe the effects of variables on the response:

$$Y = \beta_0 + \beta_1A + \beta_2B + \beta_3C + \beta_{11}X_1^2 + \beta_{22}X_2^2 + \beta_{33}X_3^2 + \beta_{12}X_1X_2 + \beta_{13}X_1X_3 + \beta_{23}X_2X_3 \dots \dots \dots (1)$$

Where, Y is the predicted response i.e., reducing sugar yield of enzymatic saccharification, β_0 is a constant; $\beta_1, \beta_2, \beta_3$ are the linear coefficients; $\beta_{11}, \beta_{22}, \beta_{33}$ are the quadratic coefficients; $\beta_{12}, \beta_{13}, \beta_{23}$ are the cross coefficients.

Statistical analysis

All the experiments pertaining to proximate analysis were carried out in triplicates with mean and standard deviation (SD) values calculated using MS Excel program.

Results and Discussion

Proximate analysis of rice straw

Pretreatment enhances saccharification rates and sugar yields of biomasses by decreasing the crystallinity of cellulose and breaking the lignin-hemicellulose sheath that surrounds the cellulose (Belal, 2013). Therefore, the rice straw was subjected to biological pretreatment i.e. ligninolytic fungal consortium consisting of *Pleurotus ostreatus* and *Phanerochaete chrysosporium*. The compositions of the rice straw before and after pretreatment were given in Table 1. The percent cellulose content increased to 56.4 % from 39.5 % of untreated rice straw. In contrast, the percent hemicellulose and lignin content after fungal consortium pretreatment

decreased to 12.2% and 2.4 % from 23.3% and 11.5%, respectively, indicating that 47.6 % and 79.1% lignin and hemicellulose can be removed by ligninolytic fungal consortium pretreatment. Similar to the present work, the rice straw has been reported to be pretreated with ligninolytic/ligninocellulolytic fungal consortium such as consortium of *Cerrena unicolor* and *Chaetomium brasiliense* (Ramarajan and Manohar, 2017); consortium of *Paenibacillus* sp. and *Aspergillus fumigatus* (Matthews, 2016). According to Liao *et al.*, (2005) either hemicellulose or lignin, prevent cellulose from being attacked by inhibiting the enzymes physically or chemically. The removal of these two fractions reduces the cellulose crystallinity and, the porosity and accessible surface area of substrate are increased, favouring the enzymatic attack (Mussatto *et al.*, 2008).

Development of a model for enzymatic saccharification of rice straw

Three independent variables viz. substrate concentration % (w/v) temperature (°C) and pH and their values at different coded and actual

levels were employed in the design matrix (Table 2). Table 3 shows the levels of selected variables for the CCD and summarizes the response values along with the predicted values.

The ANOVA was carried out to determine the significance of the model equation and the model terms (Table 4). The statistical significance of the above equation was checked by the *F* test. The model *F*-value of 130.92 and a low probability value (*P* < 0.0001) showed that the model terms were significant. The standard deviation (12.0) and coefficient of variation, which is a measure of residual variation of the data relative to the size of the mean and is inversely related to the reliability of experiment (4.48%), were reasonably low and acceptable.

The coefficient of determination (*R*²) value (0.99), a measure of the amount of variation around the mean, explained by the model indicated that only 1.0% of all variation for response could not be explained by the model and expresses a good fit. Figure 1 show that observed reducing sugars yield (the response) agreed well with the predicted data.

Table.1 Chemical composition of untreated and pretreated rice straw samples

Samples	Chemical composition (w/w, %)		
	Cellulose	Hemicellulose	Lignin
Untreated rice straw	39.5±0.20	23.3±0.21	11.5±0.17
Pretreated rice straw	56.4±3.1	12.2±0.67	2.4±0.13

Table.2 Coded values of the variables for the central composite design

Independent variables and symbols for actual values	Coded symbols	Actual values of coded levels				
		-α (-1.68)	-1	0	1	+α (+1.68)
Substrate concentration % (w/v)	X ₁	4.5	5.0	8.75	12.5	11.25
Temperature (°C)	X ₂	41.59	45.0	50.0	55.0	58.41
pH	X ₃	4.12	4.8	5.8	6.8	7.48

Table.3 Experimental design and results of CCD for saccharification of pretreated rice straw

Run no.	Variable			Response	
	Substrate concentration % (w/v)	Temperature (°C)	pH	Reducing sugars (mg/gds)	
				Observed values	Predicted values
1	2.45	50.0	5.8	236.0	246.0
2	8.75	50.0	5.8	240.0	246.0
3	8.75	50.0	5.8	252.0	246.0
4	8.75	50.0	5.8	252.0	246.0
5	12.50	55.0	4.8	408.0	410.0
6	12.50	45.0	6.8	206.0	202.0
7	5.00	55.0	6.8	168.0	158.0
8	8.75	50.0	5.8	260.0	246.0
9	8.75	41.6	5.8	274.0	278.0
10	5.00	55.0	4.8	476.0	452.0
11	5.00	45.0	6.8	160.0	158.0
12	8.75	50.0	5.8	238.0	246.0
13	12.50	45.0	4.8	354.0	334.0
14	12.50	55.0	6.8	200.0	202.0
15	8.75	50.0	7.48179	116.0	188.0
16	8.75	50.0	4.11821	460.0	402.0
17	8.75	50.0	5.8	236.0	246.0
18	5.00	45.0	4.8	380.0	378.0
19	15.05	50.0	5.8	258.0	246.0
20	8.75	58.4	5.8	334.0	342.0

Table.4 Analysis of variance (ANOVA) for the Quadratic Model with respect to saccharification of pretreated rice straw

Source	Reducing sugars (mg/gds)				
	Sum of squares	Degree of freedom	Mean square	F-value	Probability (P)> F
Model	1.791E+005	9	19898.76	130.92	< 0.0001
Residual	1519.94	10	151.99		
Lack of Fit	1052.60	5	210.52	2.25	0.1968
Pure error	467.33	5	93.47		
Cor Total	1.806E+005	19			
Standard deviation	12.0				
Coefficient of variation (CV) %	4.48				
R ² value	0.99				
Adjusted R ² value	0.98				
Predicted R ² value	0.95				
Adequate Precision	41.32				

Table.5 Significance of coefficients for the response model with respect to saccharification of pretreated rice straw

Model terms	Reducing sugars (mg/gds)			
	Coefficient Estimate	Standard error	F-value	P-value
β_0	245.94	5.03		
β_1	1.54	3.34	0.21	0.6547
β_2	18.52	3.34	30.81	0.0002 ^a
β_3	-107.09	3.34	1030.48	< 0.0001 ^a
β_{11}	2.83	3.25	0.76	0.4034
β_{22}	22.99	3.25	50.10	< 0.0001 ^a
β_{33}	17.33	3.25	28.47	0.0003 ^a
$\beta_1 \beta_2$	-7.00	4.36	2.58	0.1394
$\beta_1 \beta_3$	21.50	4.36	24.33	0.0006 ^a
$\beta_2 \beta_3$	-18.50	4.36	18.01	0.0017 ^a

^ap value less than 0.05 indicates model terms are significant

Table.6 Effect of variable's interaction on enzymatic saccharification of pretreated rice straw

Variable/Response	Goal	Lower limit	Upper limit	Predicted value	Actual value
A(Substrate concentration)	In range	5.0	2.5	12.5	NA
B (Temperature)	In range	45.0	55.0	55.0	NA
C (pH)	In range	4.8	6.8	4.8	NA
Reducing sugars (mg/gds)	Maximize	116	476	460.2	476.0 ±26.18

Table.7 Enzymatic saccharification conditions and yields from various studies on lignocellulosic biomasses

Substrate	Pretreatment	Reducing sugar yield (mg/gds)	Enzyme used	Reference
<i>Parthenium</i> sp.	Fungal	485.6	Accellerase 1500	(Rana <i>et al.</i> , 2013)
Giant reed	Dilute sulphuric acid	481.6	Celluclast 1.5 L and Novozyme-188	(Shatalov <i>et al.</i> , 2012)
Switch grass	Dilute sulphuric acid	440.0	Commercial cellulase	(Ruan <i>et al.</i> , 2013)
Rice hull	Alkaline peroxide	154.0	Celluclast 1.5 L and Novozyme 188	(Saha and Cotta 2008]
Rice straw	Steam explosion	132.0	Celluclast 1.5L, <i>Periconia</i> sp. bcc2871	(Harnpicharnchai <i>et al.</i> , 2009)
Rice hull	Lime	428.0	Celluclast, Novozyme 188 and Viscostar	(Saha and Cotta 2008)
Corn stover, <i>Miscanthus</i> and wheat straw	Sodium hydroxide	215, 258, and 280, respectively	Cellulase Onozuka	(Vintila <i>et al.</i> , 2010)
Rice straw	Fungal consortium	492.0	Arrowzyme	Present study

Figure.1 The predicted versus actual plot for reducing sugar response

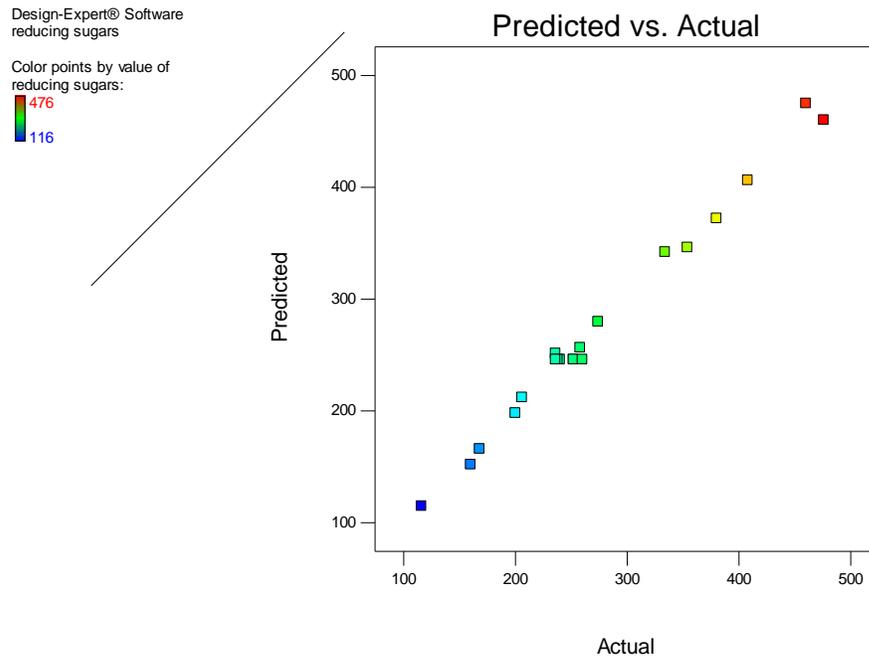
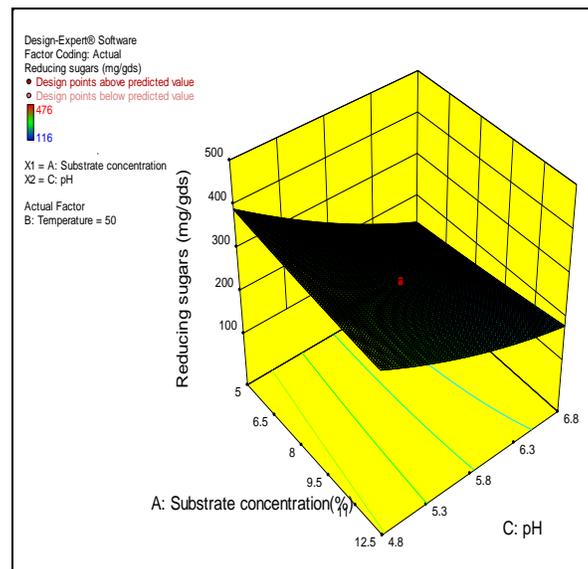
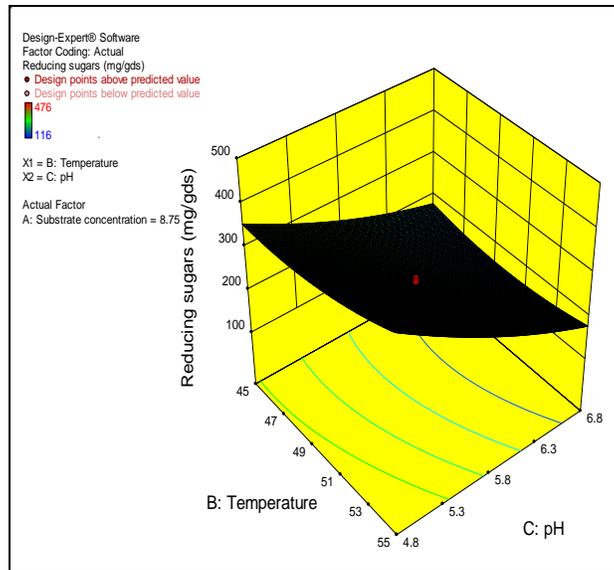


Figure 2 The 3-D response surface plots showing effects of various parameters on enzymatic saccharification of rice straw



2(a)



2(b)

Figure.3 Normal probability of internally studentized residuals for reducing sugars

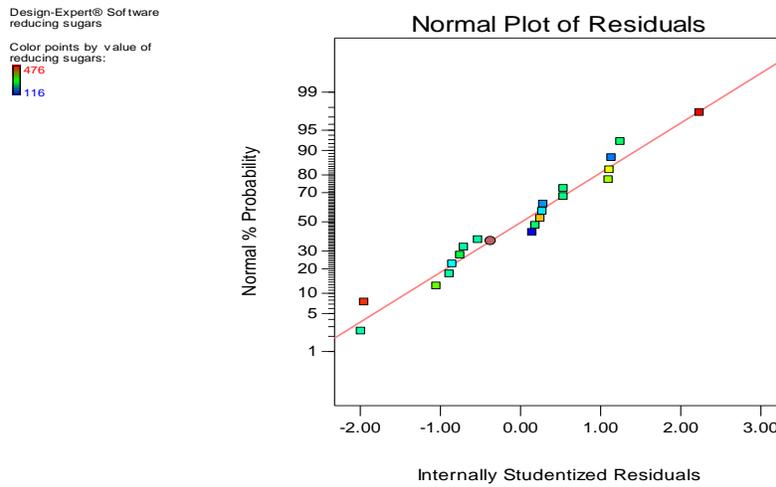
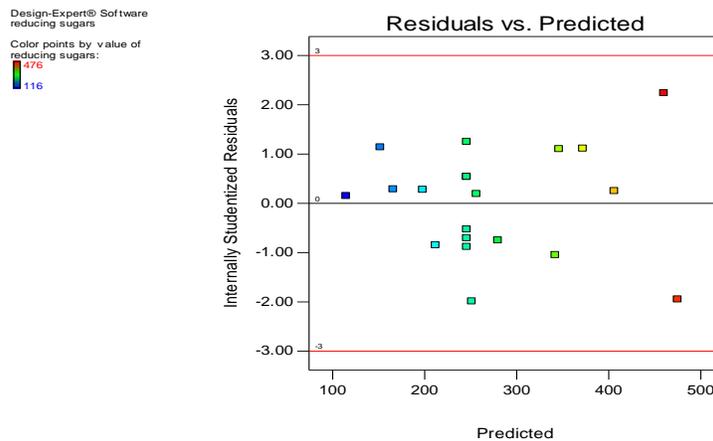


Figure.4 Plot of internally studentized residuals versus predicted response



For the developed model, the 'predicted coefficient of determination', R^2 value of 0.95 was in reasonable agreement with the 'adjusted coefficient of determination', R^2 value of 0.98. This indicated a good adjustment between the observed and predicted values. 'Adequate precision' represents the signal-to-noise (S/N) ratio and values >4.0 indicate that the model precision is Adequate. 'Adequate precision' ratio of 41.32 indicated an adequate signal.

Table 5 shows the F -test and the corresponding P -value along with the parameter estimate. The smaller the p -values, the bigger the significance of the corresponding coefficient. The parameter estimates and the corresponding p -values suggest that, among the independent variables, X_2 (temperature), and X_3 (pH) have significant effects on reducing sugars yield. The quadratic terms of X_2 , and X_3 and interactions between X_1 and X_3 , X_2 and X_3 have significant effects on reducing sugars yield. A statistically significant model only with significant terms can be written as follows:

$$Y=245.94+18.52*X_2+107.09*X_3+21.50*X_1X_3-18.50*X_2X_3+22.99*X_2^2+17.33*X_3^2 \text{ Equation 2}$$

Where Y = reducing sugar yield, X_1 -substrate concentration % (w/v), X_2 -temperature ($^{\circ}C$) and X_3 - pH

Effect of interaction of variables on reducing sugars yield

To examine the interaction of the variables and to determine the optimum level of each variable for maximum response, 3-D response surface curves were plotted against two experimental factors while maintaining the other factor constant at its central value. The two significant interactions (substrate concentration versus pH and temperature versus pH) are presented in Figure 2. The effect of interaction of substrate concentration and pH, when temperature is at central level ($50^{\circ}C$) is shown in Figure 2(a). The reducing sugars increased with increase in substrate concentration up to 5.0 % (w/v) and pH to 4.8, after which a decrease in the reducing sugars was observed. Enzymes possess ionic groups on their active sites which function in a suitable environment (acid or base). A change of pH in the

medium leads to modification of enzyme in the ionic form of active site and its three-dimensional shape, as a result of which enzymes are active over a certain pH range. Most hydrolytic enzymes work best between the pH range of 3-5, with best performance of cellulase enzyme observed at pH 5 (Shuler and Kargi, 1992). Phuengjayaem *et al.*, (2014) studied the effect of pH on saccharification of sweet sorghum bagasse and observed that maximum of 0.115 g glucose/g of dry solid was obtained at pH 5. Increased consistency, product inhibition and reduced surface contact between the enzyme and the substrate are responsible for the low reducing sugars content at high substrate concentrations. The extent of substrate inhibition is dependent on the ratio of the total substrate to total enzyme loaded (Xin *et al.*, 2010; Wang *et al.*, 2011). The effect of interaction of temperature and pH, with a substrate concentration (8.75%, w/v) at central level is presented in Figure 2 (b). The release of reducing sugars increased with an increase in temperature to $55.0^{\circ}C$ from $45^{\circ}C$ and decrease in pH to 4.8 from 6.8. This could be explained on the basis of gain of kinetic energy by the reactant molecules with increase in temperature and hence a more productive collision per unit time, resulting in better yields at high temperature (Segel, 1976). Shah *et al.*, (2016) optimized the conditions for saccharification of laccase pretreated empty fruit bunch by RSM at enzyme concentration, 30 FPU/g; substrate concentration, 5.0% (w/v); temperature, $50^{\circ}C$; saccharification time, 24 h and pH 5, resulting in highest total sugars yield of 28.0% (w/w). The optimum parameters obtained for the hydrolysis of rice straw with cellulase from *Aspergillus niger* were pH 6.0; substrate concentration, 12% (w/v) and enzyme concentration, 10 U/g of rice straw. Under the optimum conditions, fermentable sugar content of 3.62g/l was obtained (Ong *et al.*, 2012). Lai *et al.*, (2016) reported the optimization of glucose production from ammonia pretreated oil palm trunk biomass via saccharification using two commercial enzymes namely, celluclast 1.5 (cellulase) from *Trichoderma reesei* and Novozyme 188 (β - glucosidase) from *Aspergillus niger*, with the help of RSM. Under the established optimum conditions of temperature, $44.23^{\circ}C$; pH 5.22 and enzyme ratio, 3:1, a maximum glucose yield of 4.964 g/l was obtained which was in close agreement with the value of

4.958 g/l predicted by the model.

Optimization of reducing sugars yield of rice straw

Numerical optimization of saccharification process was carried out using Design Expert software, version 9.0.4.1, to evaluate the optimum values of different parameters from the developed model. In optimization, the desired goal was to maximize the reducing sugar yield with highest importance and the factors were selected to be within the mentioned range. The desirability values vary between 0 and 1 depending upon the proximity between predicted and the actual values. In the present experiment, a desirability of 0.956 was obtained. Response analysis predicted the maximum reducing sugars yield under the optimum process conditions i.e. when substrate concentration was 5.0% (w/v), temperature was 55° C and pH was 4.8 (Table 6). Validation experiment under these predicted optimum conditions yielded 476.0 mg/gds reducing sugars experimentally which was close to the predicted reducing sugars yield of 460.0 mg/gds. Thus, overall good agreement was observed between experimentally determined/observed responses and predicted optimum response.

Confirmation of adequacy of model

The residuals from the least squares are an important tool for judging the model adequacy to ensure that it provides maximum approximation on the relationship between factors and response. Normal probability was checked by plotting the normal probability plot of residuals. The normality assumption was satisfactory as normal residuals fall along a straight line as shown in Fig. 3. Figure 4 is the plot of residuals versus the predicted response. The residual plots of the model were randomly distributed without any trends which indicated good predictions of maximum response adequacy of the quadratic models.

Effect of surfactant

To enhance the rate of saccharification, Tween 20 (0.2%) was added in the experimental flask, which resulted in reducing sugar yield of 492.0

±27.06 mg/gds compared to 460±25.3 mg/gds reducing sugars without surfactant addition. The final saccharification efficiency achieved from pretreated rice straw was 81.1%. Non-ionic surfactants like Tween 20 have proven to be effective in increasing cellulose hydrolysis. The mechanism underlying the enhancement of enzymatic cellulose hydrolysis is the increase of effective cellulosic surface area as well as increase in enzyme stability by reducing thermal denaturation [Kaar and Holtzapfle, 1998; Erickson *et al.*, 2002]. For the saccharification of dilute acid pretreated rice hulls, addition of Tween 20 at 2.5g/L concentration enhanced the rice hulls saccharification by 3.5% (Saha *et al.*, 2005). In another study, addition of Tween 80 resulted in increase in hydrolysis yield from 69 to 91% after 48 h for pretreated Lodgepole pine (Tu *et al.*, 2009).

Comparison of enzymatic saccharification conditions and yields with other lignocellulosic biomass

The saccharification yield during enzymatic hydrolysis of different lignocellulosic biomass as reported by other workers is summarized in Table 7. The results revealed rice straw as a potential substrate in yielding highest amount of sugars under optimized conditions.

The present study highlights the primacy of rice straw as a feedstock for bioethanol production as well as confirms the validity of RSM as compared to conventional methods of optimization. The pretreatment of rice straw by fungal consortium have the additional advantage of obtaining cellulose rich substrate in an eco- friendly way. In addition, use of rice straw substrate, an abundantly available agricultural residue without overhead costs makes the finding of this investigation a promising approach for bioethanol production.

Acknowledgment

The authors thank Mr. Shivkaran, Technical Service Manager, Nature Bioscience Pvt. Ltd., New Delhi for kindly providing the Arrowzyme.

References

- Belal, E. B., 2013. Bioethanol production from rice straw residues. *Brazilian Journal of Microbiology* 44: 225-234.
- Binod P., R., Sindhu, R. R. Singhania, S. Vikram, L. Devi, S. Nagalakshmi, N. Kurien, R.K. Sukumaran, and A. Pandey. 2010. Bioethanol production from rice straw: An overview. *Bioresource Technology* 101:4767–4774.
- Box, G.E.P., W.G. Hunter, J.S. Hunter. 1978. *Statistic for experimenters: An introduction to design, data analysis and model building*. New York: John Wiley and Sons Inc.:p. 653.
- Desai, S. S., G. B. Tennali, N. Channaur, A. C. Anup, G. Deshpande, and B. P. A. Murtuza. 2011. Isolation of laccase producing fungi and partial characterization of laccase. *Biotechnology Bioinformatics and Bioengineering* 1: 543-549.
- El-Ahmady El-Naggar N., S. Deraz, and A. Khalil. 2014. Bioethanol production from lignocellulosic feedstocks based on enzymatic hydrolysis: Current Status and Recent Developments. *Biotechnology* 13: 1-21.
- Erickson, T., J. Borjesson, and F. Tjerneld. 2002. Mechanism of surfactant effect in enzymatic hydrolysis of lignocelluloses. *Enzyme and Microbial Technology* 31:353-364.
- Goering, H. K., and P. J. Van Soest. 1970. Forage fiber analyses (apparatus, reagents, procedures, and some applications). *Agriculture handbook no. 379*, Agriculture Research Service USDA, Washington (DC), USA. pp 20.
- Harnpicharnchai, P., V. Champreda, W. Sornlake, L. Eurwilaichitr. 2009. A thermotolerant [beta]-glucosidase isolated from an endophytic fungi, *Periconia* sp., with a possible use for biomass conversion to sugars. *Protein Expression and Purification*. 67: 61-69.
- Kaar, W. E., and M Holtzapple. 1998. Benefits from Tween during enzymic hydrolysis of corn stover. *Biotechnology and Bioengineering* 59:419–427.
- Kocher, G.S., P. Kaur, and M.S. Taggar. 2016. An overview of pretreatment processes with special reference to biological pretreatment for rice straw delignification. *Current Biochemical Engineering*. doi: 10.2174/221271190366616110214 1859
- Lai, J., S. S. M. Yahya, N. M. Nor, M R Sulong. 2016. Enzymatic saccharification on ammonia pretreated oil palm trunk biomass for glucose production: an optimization using response surface methodology. *Malaysian Journal of Analytical Science* 20: 21-30.
- Li, B. Z., V. Balan, Y.J. Yuan, B. E. Dale. 2010. Process optimization to convert forage and sweet sorghum bagasse to ethanol based on ammonia fiber expansion (AFEX) pre-treatment. *Bioresource Technology* 10: 1285–1292.
- Liao, W., Z. Wen, S. Hurley, Y. Liu, C. Liu, and S. Chen. 2005. Effects of hemicellulose and lignin on enzymatic hydrolysis of cellulose from dairy manure. *Applied Biochemistry and Biotechnology*. 121/124:1017–1029.
- Matthews, S., 2016. Structural changes of rice straw pre-treated with *Paenibacillus* and *Aspergillus fumigatus*. *International Journal of Agriculture and Food Research* 5: 1-8.
- Miller, G. L., 1959. Use of dinitrosalicylic acid reagent for determination of reducing sugar. *Analytical Chemistry* 31: 426-428.
- Mussatto, S. I., M. Fernandes, A. M. F. Milagres, and I. C. Roberto. 2008. Effect of hemicellulose and lignin on enzymatic hydrolysis of cellulose from brewer's spent grain. *Enzyme and Microbial Technology*. 43: 124–129.
- Ong, L. G. A., C. H. Chan, and A. L. Chew. 2012. Enzymatic hydrolysis of rice straw: Process optimization. *Journal of Medical Bioengineering* 1(1): 14-16. doi: 10.12720/jomb.1.1.14-16
- Paszczynski, A., R. L. Crawford, and V. B. Huynh. 1998. Manganese peroxidase of *Phanerochaete chrysosporium*: Purification. *Methods in Enzymology*. 161: 264-270.
- Phuengjayaem, S., A. Poonisrisawat, A. Petsom, and S. Teeradakorn. 2014. Optimization of saccharification conditions of acid –pretreated sweet sorghum straw using response surface methodology. *Journal of Agricultural Science* 6:120-130.
- Pointing, S. B., 2001. Feasibility of bioremediation by white- rot fungi. *Applied Microbiology and Biotechnology* 57: 20–33.
- Qi, B., X. Chen, F. Shen, Y. Su, and Y. Wan. 2009. Optimization of enzymatic hydrolysis of wheat straw pretreated by alkaline peroxide using response surface methodology. *Industrial and Engineering Chemistry Research* 48: 7346–7353.
- Ramarajan, R., and C. S. Manohar. 2017. Biological pretreatment and bioconversion of agricultural wastes using ligninolytic and cellulolytic fungal consortia. *Bioremediation Journal*. doi: 10.1080/10889868.2017.1282937
- Rana, S., R. Tiwari, A. Arora, S. Singh, K. Kaushik, A. K. Saxena, S. C. Dutta, and L. Nain. 2013. Prospecting *Parthenium* sp. pretreated with *Trametes hirsuta*, as a potential bioethanol feedstock. *Biocatalysis Agricultural Biotechnology* 2:152–158.

- Ruan, Z., M. Zanotti, Y. Zhong, W Liao, C. Ducey and Y. Liu. 2013. Co-hydrolysis of lignocellulosic biomass for microbial lipid accumulation. *Biotechnology and Bioengineering* 110: 1039–1049.
- Saha, B. C., and M. A. Cotta. 2007. Enzymatic saccharification and fermentation of alkaline peroxide pretreated rice hulls to ethanol. *Enzyme and Microbial Technology* 41: 528–532.
- Saha, B. C., and M. A. Cotta. 2008. Lime pretreatment, enzymatic saccharification and fermentation of rice hulls to ethanol. *Biomass and Bioenergy* 32: 971–977.
- Saha, B. C., L. B. Iten, M. A. Cotta, and Y. V. Wu. 2005. Dilute acid pretreatment, enzymatic saccharification, and fermentation of rice hulls to ethanol. *Biotechnology Progress* 21: 816–822.
- Segel, I. H., 1976. *Biochemical Calculations: How to solve mathematic problem in general biochemistry*. USA: John Wiley and Sons.
- Shah, S. R., U. C. Ishmael, J. V. Palliah, M. F. F. Asras, and S. S. B. N. W Ahmad. 2016. Optimization of enzyme saccharification process of empty fruit bunch pretreated with laccase enzyme. *Bioresources* 11:5138-5154.
- Sharma, R., G. S. Kocher, R. S. Bhogal, and H. S. Oberoi. 2014. Cellulolytic and xylanolytic enzymes from thermophilic *Aspergillus terreus* RWY. *Journal of Basic Microbiology* 54:1367-1377.
- Shatalov, A. A., and H. Pereira. 2012. Xylose production from giant reed (*Arundo donax* L.): Modeling and optimization of dilute acid hydrolysis. *Carbohydrate Polymers* 87: 210–217.
- Shuler, M. I., and F. Kargi. 1992. *Bioprocess engineering basic concepts*. Prentice-Hall, Englewood Cliffs, New York, 2006.
- Tien, M., and T. K. Kirk. 1988. Lignin peroxidase of *Phanerochaete chrysosporium*. *Methods in Enzymology* 161: 238-249.
- Tu, M., X. Zhang, M. Paice, P. McFarlane, and J. N. Saddler. 2009. Effect of surfactants on separate hydrolysis fermentation and simultaneous saccharification fermentation of pretreated lodgepole pine. *Biotechnology Progress* 25:1122-1129.
- Vanderghem, C., Y. Brostaux, N. Jacquet, C. Blecker, M. Paquot. 2012. Optimization of formic/acetic acid delignification of *Miscanthus x giganteus* for enzymatic hydrolysis using response surface methodology. *Industrial Crops and Products* 35: 280-286.
- Vintila, T., M. Dragomirescu, V. Croitoriu, C. H. Vintila, S. Barbu, and C. Sand. 2010. Saccharification of lignocellulose - with reference to *Miscanthus* –using different cellulases. *Romanian Biotechnology Letters*. 15: 5498-5504.
- Wang, W., L. Kang, H. Wei, R. Arora, and Y. Lee. 2011. Study on the decreased sugar yield in enzymatic hydrolysis of cellulosic substrate at high solid loading. *Applied Biochemistry and Biotechnology* 164: 1139–1149.
- Wi, S. G., I.S. Choi, K. H. Kim, H. M. Kim, and B. Hyeun-Jong. 2013. Bioethanol production from rice straw by popping pretreatment. *Biotechnology for Biofuels* 6:166-172.
- Xin, F., A. Geng, M. L. Chen, and M. J. M. Gum. 2010. Enzymatic hydrolysis of sodium dodecyl sulphate (SDS)-pretreated newspaper for cellulosic ethanol production by *Saccharomyces cerevisiae* and *Pichia stipitis*. *Applied Biochemistry and Biotechnology* 162: 1052–1064.
- Zhu, S., W. Huang, W. Huang, K. Wang, Q. Chen, and Y. Wu. 2015. Pretreatment of rice straw for ethanol production by a two-step process using dilute sulfuric acid and sulfomethylation reagent. *Applied Energy* 154:190-196.

How to cite this article:

Pardeep Kaur, Gurvinder Singh Kocher and Monica Sachdeva Taggar. 2017. Optimization of Saccharification of Biological Pre-Treated Rice Straw by Response Surface Methodology. *Int.J.Curr.Microbiol.App.Sci*. 6(10): 1112-1123. doi: <https://doi.org/10.20546/ijcmas.2017.610.135>